

H-3 Measurement in Radioactive Wastes: Efficiency of the Pyrolysis Method to Extract Tritium from Aqueous Effluent, Oil, and Concrete

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Abstract — Tritium measurement in nuclear waste is a key to determine the type of repository. This technical note describes the methodology used to validate tritium measurement in various matrices using pyrolysis method with a new instrument available in the market. The efficiency obtained for tritium recovery in aqueous matrix, oil and concrete are respectively higher than 95%, 93%, and 85%.

Keywords — Tritium measurement, oil, aqueous effluent, concrete, pyrolysis.

Note — Some figures may be in color only in the electronic version.

I. INTRODUCTION

Due to its labile and chemical behavior (organic or inorganic forms), tritium is one of the most difficult radionuclide to measure. However for Decommissioning & Dismantling (D&D) projects concerning tritium facilities, stakeholder considers its characterization as a priority.

Liquid Scintillation Counting (LSC) is the reference method for tritium measurement. In the case of solid samples usually found in D&D project, the pyrolysis method is generally used prior to measurement in order to isolate tritium from the matrix and to separate it from potential interfering species such as C-14 or S-35 (Refs. 1 through 5). As Certified Reference Materials (CRM) are rather scarce for nuclear waste materials, our analysis have been validated through proficiency tests⁶ and with homemade materials (concrete, oil). For each matrix investigated, we tried to determine the recovery yields of tritium after pyrolysis. We will present results concerning optimization of the temperature programs to obtain the best extraction of tritium from the tested liquid matrix (liquid wastes, oil and aqueous

effluents) and solid wastes (concrete). For optimizations, we also used the available CRMs proficiency tests for aqueous samples and intercomparison between laboratories for oil. For concrete, a specific study has been undertaken in order to study the influences of granulometry and sample quantity analyzed, on the recovery of H-3 after pyrolysis.

II. EXPERIMENTAL SETUP

The furnace built possesses (Fig. 1) two independent heating zones. The first, where the sample is placed, can be setup (temperature gradient) whereas the second heating zone is maintained at 950°C. Overall instrument dimensions are 1000 × 600 × 430 mm (w d h). Heating zones for each part are respectively 120 mm and 200 mm long respectively for programmable zone and constant zone. Temperature gradient can be useful for tritium speciation or tritium desorption in different matrices.² In addition, depending of the matrix where tritium has to be measured, the maximum temperature to reach for complete release of the tritium can be different from a matrix to another one. The sample in the first zone is swept by a nitrogen stream during the heat-up, while the

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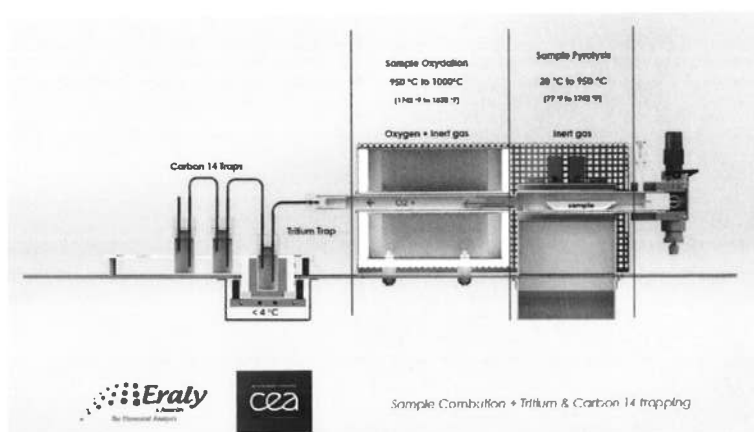


Fig. 1. Schematic view of the pyrolyser designed by ERALY and associates.

second zone had a stream of N_2 plus O_2 , in order to guarantee complete oxidation of the gases released during the pyrolysis taking place in the first zone. The sample (liquid or solid) is placed into the cold furnace in a combustion boat after a precise weighing. As the temperature rises, the gases obtained goes through a bubbler filled up with HCl 0.1 M to trap H-3. The bubbler is systematically cooled at temperature lower than 4°C for a better trapping efficiency. Difference between H-3 trapping at room temperature and a temperature below 4°C could be up to 15%.

Liquid samples are deposited on a small ceramic rod (cordierite material, porosity $> 20\%$) before pyrolysis. This ceramic is placed in the combustion boat, Fig. 2.

H-3 used for recovery experiments and optimization was certified H-3 labelled glucose (CERCA LEA, France). Tritiated oils were prepared by another CEA group (CEA valduc), and tritiated concrete was prepared with a known amount of certified H-3 glucose in water mixed manually with cement and dried for at least 3 weeks at room temperature (Fig. 3). H-3 activity ranges for concrete spread from 50 to 1000 Bq/g. Possible radiolytical conversion of tritiated glucose to HTO was not evaluated but with the recovery of H-3 observed, we can suppose that no conversion occurred.

Tritiated concrete was grinded and sieved to obtain powders with 4 different particle sizes: $\varnothing < 250 \mu\text{m}$, $250 \mu\text{m} < \varnothing < 500 \mu\text{m}$, $500 \mu\text{m} < \varnothing < 1 \text{mm}$ and

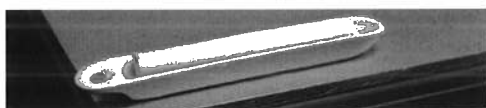


Fig. 2. Porcelain combustion boat with cordierite as sample support.

$\varnothing > 1 \text{mm}$. The powder was directly deposited in the porcelain boat before pyrolysis.

After the pyrolysis, tritium activity was measured by Liquid Scintillation Counter (LSC, TriCarb 2910Tr, Perkin Elmer). The 5 ml bubbler solution was mixed with 10 ml of scintillation cocktail (Ultima Gold LLT, Perkin Elmer). LSC counter was calibrated with a certified standard liquid source (CERCA LEA, France). The counting time is 600 seconds.

After each sample pyrolysis, a pyrolysis blank is systematically carried out without porcelain boat using the same temperature program as used for sample.

III. RESULTS AND DISCUSSION

We have optimized temperature program and gas flows for each matrix. Specifically for the concrete matrix we have studied the effect of parameters such as the total powder quantity in the porcelain boat and the particles size.

III.A. Validation on Aqueous Matrix

For aqueous matrix, the H-3 labelled glucose is diluted in water to obtain an activity around 40 Bq/g. To optimize



Fig. 3. Tritiated concrete before and after 3 weeks drying.

the temperature program in order to obtain the best recovery of tritium, 0.4 ml of this solution is deposited on the cordierite in the porcelain boat. The observation of a low influence of the gas flow rate led us to set it at 8.5 ml/min for both gases: inert gas in the first temperature programmable part of the oven and O₂ in the oven part fixed at 950°C to oxidize the released gases. The optimized temperature program obtained from different experiences is shown in Fig. 4. We can see 3 distinct stages, 350°C, 550°C, and finally 950°C. In the final part of the program, an inversion between inert gas and O₂ is proceeded to be sure that the entire sample has been oxidized.

With this pyrolysis program, a yield better than 95% with a RSD of 4% for 10 replicates has been measured for H-3.

III.B. Validation on Oil Matrix

Different temperature programs have been tested for the measurement of H-3 in oil after pyrolysis. To prevent the formation of soot, no oxygen is added in the sample part of the oven which is always under inert gas flow. The different temperature programs tested are presented in Fig. 5. For each experiment, 0.1 ml of oil is used for direct measurement and quantity between 0.1 and 0.5 ml of oil for pyrolysis. Oil used is colorless, so no color quench was observed for direct measurement by LSC.

H-3 yields obtained for each program were respectively of 94%, 45% and 25%. These recoveries are the mean obtained from 2 pyrolysis realized on the lowest and highest H-3 activities in oil (respectively 50 Bq/g and 5000 Bq/g). Independently of the obtained recovery, a big scattering is observed between the values corresponding to the two levels of activity for program 2 and 3 (> 50%), however there is a good agreement for recovery obtained with program 1 for both level of activity (< 2%). Therefore we chose

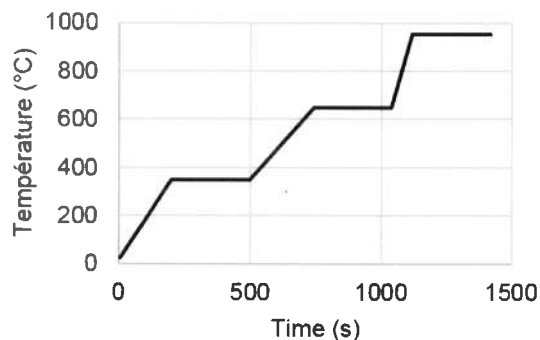


Fig. 4. Temperature program for aqueous liquid pyrolysis.

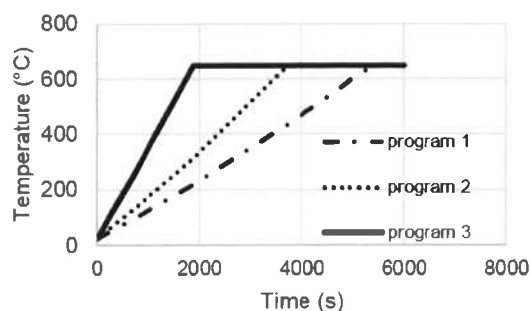


Fig. 5. Temperature programs tested for H-3 in oil matrix.

to use systematically program 1 for the validation of H-3 yield in oil and obtained a value of 93% with a RSD of 2% (10 independent pyrolysis).

III.C. Validation on Concrete Matrix

For concrete matrix, in order to optimize the temperature program and the gas flow rate to obtain the best recovery of tritium by comparison with calculation from concrete preparation, 50 mg to 300 mg with different powder grain sizes were deposited in the porcelain boat (Fig. 6).

The best experimental conditions are obtained with the same temperature program and gas flow rate as for aqueous liquid matrix pyrolysis. The best recovery is obtained for the smallest particles size, i.e. a diameter of less than 250 µm. If we have sample with high particles size, we use a step of grinding to obtain the optimum size (< 250 µm). Therefore, it was decided to study the influence of the amount analyzed in the porcelain boat for the smallest size of particles (Fig. 7). No specific experiment has been made with total amount > 300 mg because with that amount the porcelain boat is almost full.

For each quantity, we made 2 experiments (one on each pyrolysis tube for Bi tube pyrolyzer), this is considered as preliminary results before validation and determination of yields of recovery for both H-3 and C-14. We systematically obtained a H-3 recovery after pyrolysis better than 85% with a RSD of 4% for 10 pyrolysis for < 250 µm and m = 200 mg.

IV. PARTICIPATION TO INTER-COMPARISON TESTS

In 2015 our laboratory participated to an inter-comparison test organized by the Henri Becquerel National Laboratory (LNHB). Two aqueous solutions were distributed to all participants (> 30). The H-3 activity level was

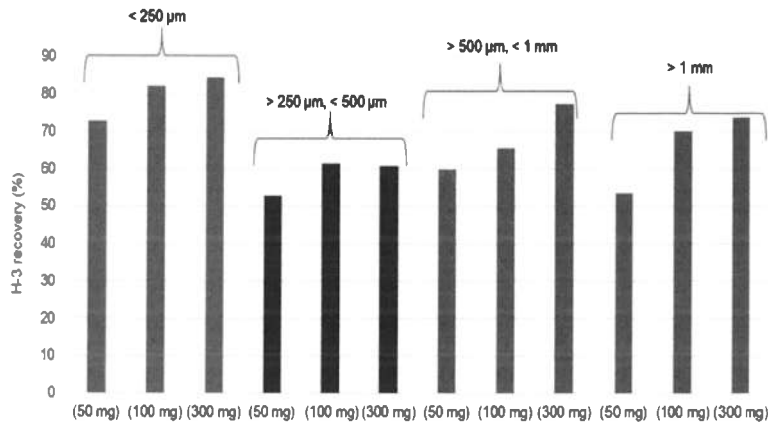


Fig. 6. Influence of the particle size on H-3 recovery, preliminary tests.

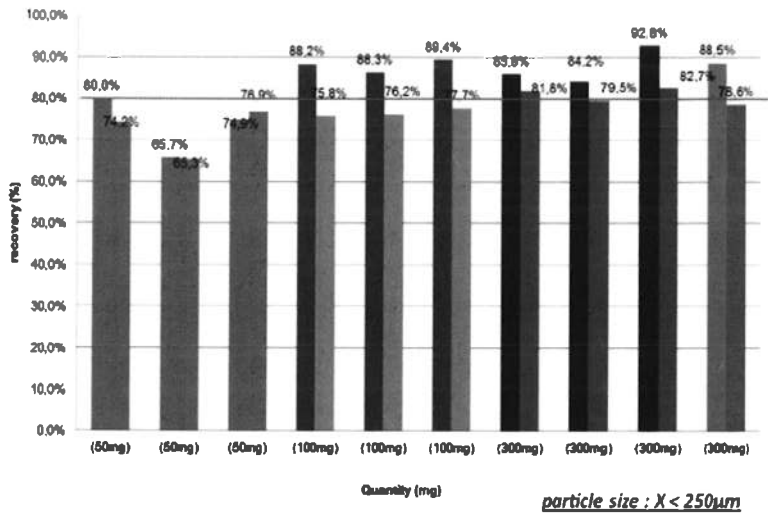


Fig. 7. Influence of the total quantity analyzed by pyrolysis for the smallest particle size on H-3 recovery, preliminary tests.

around 5 Bq/g and 40 kBq/g. Results obtained for both solutions are shown in Fig. 8.

Results obtained on aqueous solutions for both activity values show a good agreement between pyrolysis and direct measurements. For both level of activity the difference is lower than 1.6% between the reference value and the value obtained by pyrolysis. Z-score is lower than 0.6 in both cases (respectively 0.5 and 0.3).

For oil matrix, no proficiency test is available so we decided to perform inter-comparison with the laboratory able to prepare tritiated oils and compare our measurements performed after pyrolysis with direct measurement of oil by LSC. Four different levels of activity have been tested from 20 Bq/g to 5000 Bq/g. Results of these comparisons are presented in Fig. 9.

There is a very good agreement between direct measurements and H-3 measurement after pyrolysis. Uncertainty obtained for pyrolysis measurement is higher than that obtained for direct measurement because it takes into account the yield of extraction determined by pyrolysis and its uncertainty. The laboratory which prepared the labelled oil obtained the same results with both techniques but different instruments.

For concrete matrix, we had the same problematic as for oil matrix as no proficiency test is available for this type of matrix. We decided to assess our results with an internal blind test by using a concrete prepared in our laboratory with unknown H-3 activity. We obtained with the optimized conditions of pyrolysis a difference of less than 5% between theoretical and measured H-3 activity in that concrete.

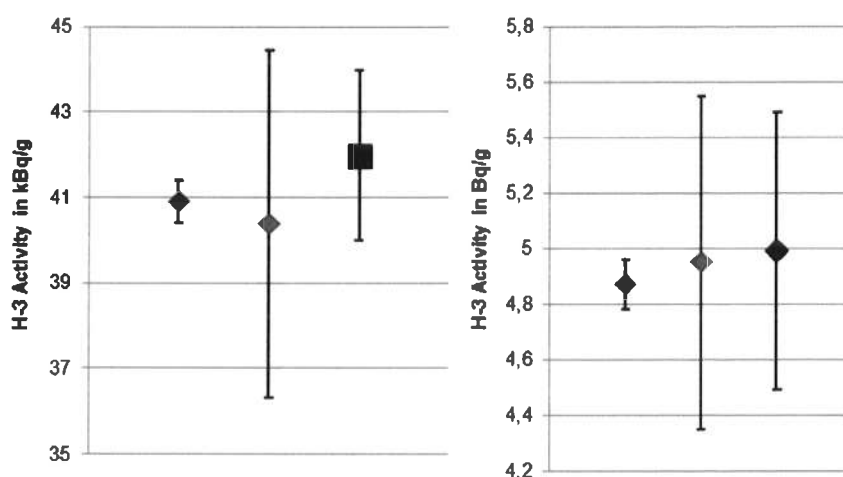


Fig. 8. Results for H-3 measurements in aqueous solution: first value is the reference value given by the LNHB, the second value is the result obtained by pyrolysis, and the third result is the direct measurement by LSC for both level of H-3 activity, uncertainty reported are for $k = 2$ (95% confidence level).

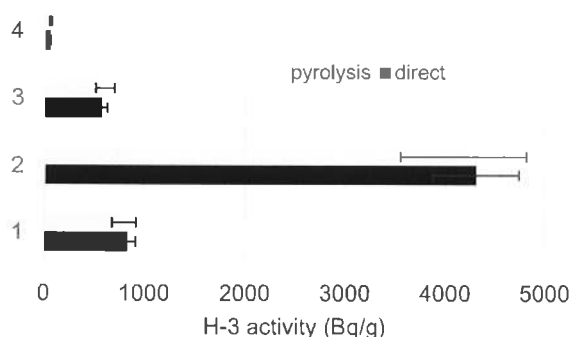


Fig. 9. Comparison between H-3 direct measurement and H-3 after pyrolysis for 4 different levels of H-3 activity in oil.

V. CONCLUSION

A new pyrolyser available on the market and designed by a small company, Eraly and Associates was tested to extract H-3 from different matrices representative of wastes that can be encountered in dismantling process. Up to 15 samples can be measured per day, H-3 and C-14 is efficiently extract without need of catalyst in the oxidation zone. Pyrolysis of aqueous matrix or concrete takes 35 minutes (3 samples in parallel), then the furnace takes 10 minutes to cool down before we can perform pyrolysis blanks. It is a total time of 1.5 hours for 3 samples. We optimized in terms of yields the operating conditions for 3 matrices: aqueous effluent, oil and concrete. We determined the best operating conditions for each matrix in order to obtain a H-3

recovery better than 85% for all matrices. In order to evaluate the technique on aqueous effluents, we participated to proficiency test organized for pure water matrice and obtained very satisfactory results. Program is going on with other matrices such as rubber and graphite.

Acknowledgments

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